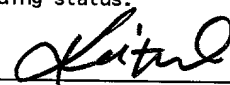


Form PTO-1390		U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE	ATTORNEY'S DOCKET NUMBER LAIN-033
TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371		U.S. APPLICATION NO. 09/674289	
INTERNATIONAL APPLICATION NO. PCT/FI99/00359	INTERNATIONAL FILING DATE April 30, 1999	PRIORITY DATE CLAIMED April 30, 1998	
TITLE OF INVENTION A METHOD OF PRODUCING A FIBER PRODUCT		DATE October 30, 2000	
APPLICANT FOR DO/EO/US Tapani VUORINEN			
<p>Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:</p> <ol style="list-style-type: none"> <input checked="" type="checkbox"/> This is a FIRST submission of items concerning a filing under 35 U.S.C. 371. <input type="checkbox"/> This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371. <input checked="" type="checkbox"/> This express request to begin national examination procedures (35 U.S.C. 371(f) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. 371(b) and PCT Articles 22 and 39(1). <input checked="" type="checkbox"/> A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date. <input checked="" type="checkbox"/> A copy of the International Application as filed (35 U.S.C. 371(c)(2)) <ol style="list-style-type: none"> <input type="checkbox"/> is transmitted herewith (required only if not transmitted by the International Bureau). <input checked="" type="checkbox"/> has been transmitted by the International Bureau. <input type="checkbox"/> is not required, as the application was filed in the United States Receiving Office (RO/US). <input checked="" type="checkbox"/> A translation of the International Application into English (35 U.S.C. 371(c)(2)) (20 pages and 4 sheets of drawings (Figs. 1-7)). <input checked="" type="checkbox"/> Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3)) <ol style="list-style-type: none"> <input type="checkbox"/> are transmitted herewith (required only if not transmitted by the International Bureau). <input type="checkbox"/> have been transmitted by the International Bureau. <input type="checkbox"/> have not been made; however, the time limit for making such amendments has NOT expired. <input checked="" type="checkbox"/> have not been made and will not be made. <input type="checkbox"/> A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371(c)(3)). <input checked="" type="checkbox"/> An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)). <input type="checkbox"/> A translation of the annexes to the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)). <p>Items 11. to 16. below concern other document(s) or information included:</p> <ol style="list-style-type: none"> <input checked="" type="checkbox"/> An Information Disclosure Statement under 37 CFR 1.97 and 1.98. <input checked="" type="checkbox"/> An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included. <input checked="" type="checkbox"/> A FIRST preliminary amendment. <input type="checkbox"/> A SECOND preliminary amendment. <input type="checkbox"/> A substitute specification. <input type="checkbox"/> A change of power of attorney and/or address letter. <input checked="" type="checkbox"/> Other items or information: <ol style="list-style-type: none"> PCT/RO/101 PCT/IB/306 PCT/IPEA/401 PCT/IPEA/409 with annexes (substitute pages 17-19, amended claims) WO 99/57370 PCT/ISA/210 			

U.S. Application No. 09/ 674289		International Application No. PCT/FI99/00359		Attorney's Docket No. LAIN-033	
				CALCULATIONS	PTO USE ONLY
17. [XX] The following fees are submitted:					
Basic National Fee (37 CFR 1.492(a)(1)-(5):					
Search Report has been prepared by the EPO or JPO \$860.00					
International preliminary examination fee paid to USPTO (37 CFR 1.482) \$690.00					
No international preliminary examination fee paid to USPTO (37 CFR 1.482)					
but international search fee paid to USPTO (37 CFR 1.445(a)(2)) . . . \$700.00					
Neither international preliminary examination fee (37 CFR 1.482) nor					
international search fee (37 CFR 1.445(a)(2)) paid to USPTO . . . \$1,000.00					
International preliminary examination fee paid to USPTO (37 CFR 1.482)					
and all claims satisfied provisions of PCT Article 33(2)-(4) . . . \$100.00					
ENTER APPROPRIATE BASIC FEE AMOUNT =				\$	1,000.00
Surcharge of \$130.00 for furnishing the oath or declaration later than [] 20 [] 30 months from the earliest claimed priority date (37 CFR 1.492(e)).					
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE		
Total claims	21 - 20	1	x \$ 18.00	\$	18.00
Indep. claims	2 - 3		x \$ 80.00	\$	0.00
Multiple dependent claim(s) (if applicable)			+ \$ 270.00	\$	0.00
TOTAL OF ABOVE CALCULATIONS =				\$	1,018.00
Reduction by 1/2 for filing by small entity, if applicable. Verified Small Entity statement must also be filed. (Note 37 CFR 1.9, 1.27, 1.28).				\$	0.00
SUB TOTAL =				\$	1,018.00
Processing fee \$130.00 for furnishing the English translation later than [] 20 [] 30 months from the earliest claimed priority date (37 CFR 1.492(f)).				\$	0.00
TOTAL NATIONAL FEE =				\$	1,018.00
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3.31). \$40.00 per property +				\$	40.00
TOTAL FEES ENCLOSED =				\$	1,058.00
				Amount to be refunded:	\$
				charged	\$
a. [XX] Check in the amount of <u>\$1058.00</u> to cover the above fees are enclosed.					
b. [] Please charge my Deposit Account No. <u>111833</u> in the amount of \$_____ to cover the above fees.					
c. [XX] The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any overpayment to Deposit Account No. <u>111833</u> . Two copies of this sheet are enclosed.					
NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to review (37 CFR 1.137(a) or (b) must be filed and granted to restore the application to pending status.					
SEND ALL CORRESPONDENCE TO: KUBOVCIK & KUBOVCIK The Farragut Building Suite 710 900 17th Street, N.W. Washington, D.C. 20006				 Signature Keiko Tanaka Kubovcik Name 40,428 Registration Number October 30, 2000 Date	

09/674289

526 Rec'd PCT/PTO 30 OCT 2000

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re the application of:

Tapani Vuorinen

Attn: Box PCT

International Application No. PCT/FI99/00359

I.A. Filing Date: April 30, 1999

U.S. Serial Number:

For: A METHOD OF PRODUCING A FIBER PRODUCT

PRELIMINARY AMENDMENT

Assistant Commissioner
For Patents
Washington, D.C. 20231

October 30, 2000

Sir:

Prior to calculation of the fee and examination on the merits of the above-identified patent application, please amend the application as follows:

IN THE CLAIMS:

Please amend claims 4-8, 10-14, 19 and 20 as follows:

Claim 4,

line 1: delete "any of claims 1 - 3" and insert therefor --

claim 1--,

Claim 5,

Claim 6,

Claim 7,

Claim 8,

Claim 10,

2

U.S. National Stage of
PCT/FI99/00359
PRELIMINARY AMENDMENT

Claim 11,

line 1: delete "any of claims 1-7" and insert therefor --
claim 1--,

Claim 12,

line 1: delete "any of the previous claims" and insert
therefor --claim 1--,

Claim 13,

line 1: delete "any of the previous claims" and insert
therefor --claim 1--,

Claim 14,

line 1: delete "any of the previous claims" and insert
therefor --claim 1--,

Claim 19,

line 1: delete "any of the previous claims" and insert
therefor --claim 1--,

U.S. National Stage of
PCT/FI99/00359
PRELIMINARY AMENDMENT

Claim 20,

line 1: delete "any of the previous claims" and insert
therefor --claim 1--.

REMARKS

Amendments under PCT Article 34 were filed on June 5, 2000, (a copy of Annexes to the Preliminary Examination Report is attached hereto). Amendments made in this preliminary amendment are to claims 1 to 21 amended under PCT Article 34.

The claims have been amended to remove multiple dependencies and to conform with standard United States Patent practice.

In the event any additional fees are required, please charge our Deposit Account No. 111833.

Respectfully submitted,

KUBOVCIK & KUBOVCIK



Keiko Tanaka Kubovcik
Reg. No. 40,428

PATENT

U.S. National Stage of
PCT/FI99/00359
PRELIMINARY AMENDMENT

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A method of producing a fiber product

The present invention relates to a method according to the preamble of claim 1 for
5 producing a fiber product. According to the method, a cellulosic raw material is formed
into a fiber suspension, into which components modifying the properties of the fibers are
introduced, subsequent to which the suspension is dried.

The invention is especially related to a method of producing a web having good strength
10 properties and a high water absorption capability.

The invention also relates to a fiber product as described in the preamble of claim 21.

It is known in prior art that the properties of the cellulose fibers used for producing paper
15 can be modified by adding polymers to the fiber suspension (pulp) prior to wire forming.
Suitable additive materials include starch-based components, such as cationed starch, and
different kinds of plastic materials, such as polyacryl polymers and polyamineamide-,
polyamine- and acrylamino-epichlorohydrine polymers. Conventionally, the amounts
added are about 0.5 - 5 % (by weight) of the pulp dry material.

20 The above-mentioned polymers can be used for increasing the dry and wet strength and
water absorption of papers. A drawback of the known methods is, however, the relatively
weak bonding between the conventional polymers and the cellulose fibers. For this reason
the materials accumulate in the water circulation of the paper machine, which causes
25 additional problems in treating and cleaning white water. Another drawback of the
synthetic materials is their bad biodegradability, which affects the recycling and
composting of the paper manufactured from the pulp.

Anionic polymers containing carboxyl groups or carboxylate ions in the form of alkali
30 metals or ammonium salts are often added to the pulp to improve the retention of the
cationic polymers. Carboxyalkylated polysaccharides, such as carboxymethyl cellulose,
CMC (see for example US patents 5,061,346 and 5,316,623) can especially be mentioned
as examples of anionic polymers. Usually, these polymers are added to the pulp in larger

quantities than the usual modifying chemicals, i.e. the amount is typically about 5 - 20 % of the fiber material content of the pulp.

5 A drawback of the mixing of cationic and anionic polymers is that they might react together and macrocoagulate, if they are added together or if the anionic polymer is introduced to the fibers before the cationic modifying chemicals. For this reason it is difficult to evenly distribute the cation polymer in the fibers. Additionally, using several different components will further affect the treatment of white water.

10 There are also prior art solutions, in which the strength properties of papers are enhanced by adding mainly only alkyl derivatives of cellulose as modifying agents. The GB patent publication 978 953 describes a method of forming a fiber web having good strength properties, according to which method a hydrophilic bonding compound is produced from cellulose ether, which is then mixed with the pulp or water phase either in swollen form or
15 as a gel. The amount of bonding compound added to the pulp can be as high as 25 % of the amount of pulp. According to the above patent publication, the method produces very even sheets, and the bonding compound increases the bonds between the fibers, thus increasing the strength of the sheet.

20 However, the solution is a complex one and difficult to apply on an industrial scale, because the cellulose ether will first have to be extruded for forming a bonding compound having a suitable composition.

US patent publication 5,275,698 describes a method of adding cellulose polymers to the
25 pulp. The cloud point of the utilized cellulose polymers is between 10 - 95 °C, and their solubility is inversely proportional to the temperature. When the polymer is added as water solution to the pulp in a temperature below the cloud point, the temperature of the pulp being higher than the cloud point of the polymer, the polymer is caused to coagulate into a colloid as it is dispersed into the pulp.

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In the method according to the US patent publication the coagulation of the polymers is difficult to control, and during introduction the pulp must be vigorously agitated in order to uniformly distribute the polymer into the fibers.

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Another considerable application for pulps produced according to the invention are soft

tissues, in which the bonded cellulose derivative will increase water retention.

The invention can also be used for producing modified fiber products that, on account of their good water retention, can be used in hygiene products, such as diapers.

5

According to the invention, the sorption can be even achieved essentially without separate retention chemicals, even though they can also be used. Preferably, an amount in excess of 50 % of the cellulose derivative in the solution will be bonded into the fibers.

10 In the following, the invention will be discussed in more detail using a detailed description of the invention and some working examples.

The following drawings graphically illustrate test results of pulps treated with CMC and, correspondingly paper sheets made from these pulps, in which

15 figure 1 illustrates the CMC content of fibers using different refining grades,
figure 2 illustrates the results of water retention tests,
figure 3 illustrates the filtration times of pulp,
figure 4 illustrates the total retention of the pulp,
figure 5 illustrates the opacity of the paper as a function of tensile index,
20 figure 6 illustrates the air permeability of the paper as a function of tensile index,
figure 7 illustrates the internal bond strength of the paper as a function of density.

The invention is exemplified by using carboxymethyl cellulose and its sorption into cellulose pulp as an example. Even though CMC represents an especially preferred
25 embodiment, it is to be noted, that the principles described in the invention can also be applied for other cellulose derivatives, such as methyl cellulose, hydroxyethyl cellulose and hydroxypropyl cellulose, that are similar in the respect of bonding. The properties, for example strength and/or water absorption, of cellulose fibers can be modified by means of these derivatives.

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In the examples described below, the solution according to the invention is used for modifying the fibers of chemical pulp. In this context, chemical pulp means pulp that has been treated with cooking chemicals for delignifying the cellulose fibers. According to an

advantageous embodiment of the invention, the invention is applied to pulps produced with sulphate process and other alkaline processes. "Sulphate process" in this context means a cooking method in which the main cooking chemicals are sodium sulphide and sodium hydroxide. Extended cooking, in which a conventional sulphate process is continued until the kappa value of the pulp is below 20, can be mentioned as an example of other alkaline processes. Typically, these methods include oxygen treatment. The invention can as well be used for modifying the properties of pulps produced with acid cooking methods. Peroxo-alkane acid cooking can be mentioned as an example of acid cooking methods.

- 10 In addition to chemicals pulps, the present invention is suitable for modifying chemi-mechanical and mechanical pulps.

According to the invention, the cellulose derivative (described in the following as CMC) is introduced in liquid phase to contact the fibrous material, and the contact is continued until the cellulose derivative is bonded (sorbed) to the cellulose pulp so that it can not be washed off. The cellulose derivative can be added as solids directly to the pulp containing fibrous material, whereby the pulp is subjected to efficient dispersion to dissolve the CMC. However, it is more efficient to perform contacting by first forming a water or alkaline solution from the CMC, with the solution being mixed with the pulp containing fibrous material. This kind of solution or suspension is homogenized in room temperature or elevated temperature (<100 °C), insoluble material is separated either centrifugally or by filtration, and the clarified main solution is recovered and used for bonding.

At least 10 %, preferably at least 20 %, especially preferably at least 30 % and most preferably at least 50 % by weight of the cellulose derivative in the bonding solution, is dissolved in water or water phase in the alkaline conditions of the sorption.

When performing the invention, an essential portion of the CMC in alkaline or water solution is being subject to bonding so that at least 10 % by weight, preferably at least 30 % by weight, especially preferably at least 40 % by weight and most preferably at least 50 % by weight (or even considerably more: 60 - 95 % by weight) of the CMC is bonded from the solution to the fibers.

During testing we noticed that sorption takes especially place, if the CMC is not too soluble in water in neutral conditions. Degree of substitution (DS) of conventional CMC grades is too high (typically 0.5 - 0.6) for achieving sufficient bonding. Therefore, the present invention utilizes CMC grades with a DS below 0,5. In this context, the degree of substitution means the amount of substituted hydroxyl groups per anhydro-glucose unit. In neutral conditions, the water solubility of these CMC grades is about 20 weight-% at the most, preferably about 10 weight-% at the most, most preferably about 0 - 5 weight-%.

According to an advantageous embodiment of the invention, the used material is CMC, which is water-soluble in mainly alkaline conditions. The degree of substitution of these derivatives is, for example, about 0.2 - 0.3, whereby CMC is bonded in alkaline conditions, typically in pH value 8 - 13, or in the area of $0.3 < \text{pH} < 0.5$, whereby bonding can even be accomplished in neutral conditions. Generally, the advantageous degree of substitution for the invention can be defined as about 0.2 - 0.4. CMC used in the invention is completely water-soluble in alkaline conditions or the alkaline solution contains only a small amount of insoluble residues causing turbidity. Generally, at least 80 weight-%, preferably at least 90 weight-% and especially at least 95 weight-% of the CMC is soluble in alkaline conditions mentioned above.

The alkaline solubility of CMC makes it possible that CMC first can be dissolved in an alkaline solution, subsequent to which the ordinary bonding can take place in essentially neutral conditions at a pH value of about 6 - 12, preferably about 7 - 10.

Another important factor controlling the bonding of CMC is its molecular weight. If the molecular weight is high, the bonding only occurs on the outer surfaces of the fibers. This kind of modification allows enhancing of the strength properties of the fibers. CMC grades with smaller molecules can, on the other hand, penetrate the internal cells of the fiber wall, which also increases the amount of bonded CMC.

According to an advantageous embodiment of the invention CMC with a degree of polymerization (DP) of about 100 - 5000, especially preferably about 600 - 4000, is used. CMC having a low DP can be bonded into the fiber in greater quantities, which can have an advantageous effect on, for example, water absorption and degree of reservation of the

fiber.

Commercially available CMC grades can be used for carrying out the invention, the CMC's having a suitable degree of substitution and molar mass. When necessary, the properties of CMC can be modified in liquid phase prior to mixing it with the fibrous material in the pulp (i.e. fiber suspension). It is especially advantageous to disintegrate CMC for lowering its molar mass. In an advantageous embodiment of this option CMC is first dissolved or suspended into water or alkaline solution, subsequent to which material is added into the liquid phase for chemically or enzymatically fragmenting the anhydroglucose chain of the CMC for producing a CMC with a decreased molar mass. Examples of suitable materials include hydrogen peroxide and other radical producers. If necessary, the disintegration can be enhanced by using a catalyst.

According to an advantageous embodiment of the invention CMC is disintegrated to decrease the viscosity of its water or alkali solution. Most suitably the viscosity is decreased by at least 20 %, advantageously 50 - 90 %. Reducing the viscosity to one third produces a CMC product that bonds considerably stronger than untreated CMC.

For the bonding, the pH of the fiber suspension is set to the above-mentioned value of 6 - 13, preferably to 6 - 10. A suitable base or acid is used for setting the pH. Preferably, bicarbonate or carbonate of alkali metal or alkali metal hydroxide are used as bases. Mineral acid or an acid salt is used as the acid. Sulphuric acid and its acid salts, such as alum, are considered the most suitable salts, and sodium bicarbonate, sodium carbonate and sodium hydroxide are considered the most suitable bases.

The fiber suspension and cellulose derivative are mixed for at least 1 minute, preferably for at least 5 minutes, especially preferably for at least 10 minutes and most preferably for 20 minutes before drying (for example web forming). If a high degree of bonding is desired, mixing times of several hours, such as from 1 hour to 10 hours, are possible. Temperature is not a critical factor, in unpressurized conditions the temperature is typically 10 - 100 °C, preferably about 20 - 80 °C. The amount of the cellulose derivative is 0.1 - 5 % by weight of the cellulose fibers.

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attained. The alkaline filtrate used in the bonding stage can be introduced to P stage, where the CMC present in the filtrate can be sorbed on the surface of the mechanical mass, thereby increasing the bonding characteristics thereof.

- 5 The bonding of the cellulose derivative can be performed as a batch or semi-batch process or as a continuous process by first arranging the pulp retention time to be sufficiently long for the utilized process apparatus. A continuous process is considered advantageous.

- 10 The fiber pulp is formed into a web using a paper or a paperboard machine in a way known per se. Usually, the thickness of the web is 30 - 500 g/m². Soft tissues can be mentioned as examples of especially advantageous paper products.

The fiber suspension can also be dried for producing an absorbent fiber material used in, for example, hygiene products, such as diapers.

- 15 The amount of cellulose derivative that can be washed away from a CMC treated fibrous raw material after alkali displacement and water washing is about 10 %, at the most, at a temperature of 25 °C and neutral pH conditions. CMC is not removed during beating, either. When utilizing the present invention, the strength properties can be considerably
20 improved according to the molar mass of CMC. When compared with untreated paper, the same internal bond strength can be achieved while reducing the amount of pulp amount at least 10 %.

- CMC, when sorbed according to the invention, will increase the characteristic bond
25 strength of the fibers. This means that a certain strength level can be achieved with a lower bonding level. Low bonding level, on the other hand, leads to advantageous properties, such as high opacity (printing papers) or good air permeability (packing materials). High water retention can be achieved already with a low amount of large-molecule CMC as long as the pulp is beaten before sorption.

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In the following, the present invention is discussed in more detail using the following non-limiting embodiment examples.

Example 1

Sorption of carboxymethyl cellulose into pulp fiber

CMC was sorbed into sulphate pulp, both unbeaten and PFI beaten with different
 5 revolutions. The utilized pulp was ECF bleached softwood sulphate pulp produced by
 Kaukaa, with dry solids content of 50 %. The cold disintegration of the pulp was
 performed according to the standard method SCAN-C 18:65. The pulp was beaten with a
 PFI beater equipped and calibrated according to the standard method SCAN-C 24:67, the
 numbers of revolutions used were 1000, 2000, 4000 and 7000. After the beating, the
 10 Schopper-Riegler value of the pulps were determined according to the standard method
 SCAN-C 19:65 and the Canadian Freeness value was determined according to the standard
 method SCAN-C 21:65. The results are presented in table 1.

Table 1. SR and CF numbers for pulps beaten for different numbers of revolutions.

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PFI beating (revolutions)	SR value	CF value
0	14.5	710
1000	15	680
2000	16	660
4000	20	550
7000	36	310

Carboxymethyl cellulose (Nymcel ZSB-10, F1226) having a substitution level of 0.20 was
 30 sorbed into the above-mentioned pulps using a rotating 8 liter pulp digester. The
 temperature was elevated to 60 °C in 20 minutes, and the temperature was kept at this level
 for an hour. pH of the sorption solution was 12.5, and the consistency of pulp used for the
 sorptions was 5 % (50 g/l). In the beginning of the sorption the CMC content was 0.5 g/l (1
 % of fiber). After sorption, the pulp was cooled, filtered and washed, until its pH was 6.
 35 Reference pulps were produced in the same conditions, without the CMC addition, as the
 CMC treated pulps.

The amount of CMC sorbed into the fiber was analyzed by determining the amount of
 CMC present in the solution after sorption. The CMC content of the sorption solution was
 40 determined by means of a phenolsulphur acid test using a glucose standard line, and the
 amount of CMC present in the fibers was calculated on the basis of the CMC loss of the

solution. The results are shown in figure 1.

As the figure shows, about a half of the used CMC (about 0.5 % of fiber) was sorbed into the unbeaten fibers, and the CMC content of the fibers increased along with the beating
 5 level of the pulp, i.e. almost all of the CMC (about 1 % of fiber) was sorbed into the pulp beaten for 4000 revolutions.

Comparison example

Adding starch to the pulp

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A batch of starch-modified pulp was also produced for comparing the properties of CMC pulp. The used starch was kationic potato starch ether Raisamyl 135, with a substitution level of 0.035. The starch was introduced to the pulp as a 0.5 % solution, the pulp having a consistency of 3 %. The amount of starch was 0.5 % of the amount of fiber. Starch was
 15 introduced both to unbeaten pulp and pulp treated with PFI beating for 4000 revolutions.

Example 2

Testing the pulp

20 Methods

1. SR and CF values of pulp

The Schopper-Riegler value was redetermined after treatments according to the standard
 25 method SCAN-C 19:65 and the Canadian Freeness value was determined according to the standard method SCAN-C 21:65.

2. Water retention of fiber

30 The water retention of the fiber was analyzed by means of WRV determinations according to the proposed standard method SCAN-C 102 XE (4nd proposal). WRV determinations were performed using a Jouan GR 4 22 centrifuge.

3. Drainage properties

The drainage time of the pulp was determined using a DDA apparatus (Dynamic Drainage Analyser) manufactured by AKRIBI Kemikonsulter Ab. The used sample volume was 750 ml, the consistency of the sample was 0,6 % for pulps beaten for both 1000 and 2000 revolutions; for pulps beaten for 4000 and 7000 revolutions the consistency of sample was 0,2 %. The used partial vacuum was 0.14 bar. The used wire was delivered by the manufacturer, M 0,150 T 0,112.

4. Total retention

The total retention was analysed using a DPCJ apparatus (Dynamic Paper Chemistry Jar). The sample volume was 500 ml, the consistency of the sample was 0.2 %, and the agitation speed was 1000 krpm. The wire used in total retention determination was a 75 mesh wire.

The results of the water retention testing are shown in figure 2, the drainage times of the pulp are shown in figure 3 and the total retention of the pulp is shown in figure 4.

As the appended figures illustrate, the water retention of CMC treated pulps increased considerably in proportion to the amount of beating prior to sorpting the CMC. The water retention of a CMC treated pulp beaten for 2000 revolutions was already double the retention of corresponding reference pulp. The results point to the conclusion that a CMC treated pulp beaten to a high SR value is extremely suitable for producing of, for example, soft tissues.

The drainage time given in figure 3 is the period of time from the start of the determination to the point when air begins to be sucked to the wire through the formed sheet. The air permeability of the formed wet sheet was measured 60 seconds after the drainage time.

Figure 3 illustrates that CMC treated pulps were slower to drain than the corresponding reference pulps while forming a denser sheet than the reference sheets. We wish to point out at this point that even though the CMC treated pulps were thus slower to drain than the reference pulps having same beating level, the drainage was considerably faster when the

tensile strength was equal.

Figure 4 illustrates that the sorption of CMC to the pulp fibers does not have substantial effect on the retention of the pulp, but the total retentions of both the CMC treated pulps and the reference pulps beaten to a certain level were highly similar. Nevertheless, when the tensile strength levels are equal, the retention of the CMC treated pulps was better than that of the reference pulps.

Example 3

10 Production of laboratory sheets

Laboratory sheets were produced from the pulp samples for testing the technical properties of paper. The laboratory sheets were produced without white water according to the standard method SCAN-C 26:76 with the exception of drum drying (2 h, 60 °C) and the wet pressing (490 kPa) preceding it.

The grammage, thickness and density of the paper were measured from the laboratory sheets according to the standard methods SCAN-P 6:75 and SCAN P 7:75. The results are presented in table 2.

Table 2. Specifications describing the common properties of the paper

	Sample	PFI beating	Grammage (g/m ²)	Thickness	Density
		(revolutions)		(μm)	(kg/m ³)
25	REF	0	60.8	126	483
		1000	65.2	117	559
30	CMC	2000	65.1	107	606
		4000	62.6	96.6	648
35		7000	60.7	87.6	693
		0	66.8	125	533
	CMC	1000	67.3	110	611
40		2000	64.7	101	639
		4000	64.8	98.6	657
45		7000	65.4	94.3	694
	Raisamyl	0	62.9	128	492
		4000	67.6	97.7	691

As the table describes, the densities of sheets produced from unbeaten and only slightly beaten CMC treated pulps were considerably increased when compared with the corresponding reference pulps. In the sheets produced from more extensively beaten pulps (4000 and 7000 revolutions) the density increase caused by CMC sorption was not significant.

Example 4

Properties of laboratory sheets

1. Optical properties

The optical properties of sheets produced according to example 3 (ISO lightness, opacity, light-scattering coefficient, light absorption coefficient) were determined using an Elrepho reflectometer equipped and calibrated according to the standard method SCAN-G 1:75.

The measured light-scattering values were used for calculating the relative bonded area, RBA describing the bonding level. The results are presented in table 3.

Table 3. Specifications describing the optical properties of the paper

Sample	PFI beating (revolutions)	ISO lightness (%)	Opacity (%)	Light-scattering coefficient (m ² /kg)	RBA (%)	Light absorption coefficient (m ² /kg)
REF	0	86.1	72.3	32.7	13.4	0.129
	1000	85.5	70.5	27.4	27.4	0.141
	2000	84.5	66.8	23.6	37.5	0.132
	4000	83.7	62.6	20.6	45.4	0.140
	7000	82.3	58.3	17.5	53.6	0.156
CMC	0	86.2	71.8	29.0	23.2	0.121
	1000	84.9	68.5	24.2	35.9	0.141
	2000	83.7	64.5	20.9	44.6	0.155
	4000	82.6	61.4	18.2	51.8	0.164
	7000	81.8	57.4	15.6	58.7	0.145
Raisamyl	0	86.5	71.6	30.8	18.4	0.121
	4000	82.6	60.8	17.4	53.9	0.138

Thus, the lightness and opacity of the sheets produced from CMC treated pulps was higher than those of the reference sheets having the same tensile strength. This is also clearly

shown in the appended figure 5, in which opacity is shown as a function of tensile index.

2. Roughness and air permeability

- 5 The roughness and air permeability of the paper were determined with a Bendtsen apparatus calibrated according to the standard method SCAN-P 21:67. The apparatus was equipped with both an air permeability measuring sensor and a roughness measuring sensor. In figure 6, the air permeability describing the porosity of the paper is shown as a function of tensile index. The figure illustrates that the laboratory sheets produced from
- 10 CMC treated pulp having a certain tensile strength were considerably more porous than corresponding laboratory sheets produced from reference pulps.

3. Mechanical properties

- 15 The tensile strength, stretch at break and tensile breaking load were determined using an MTS 400M -stretching apparatus, the distance between the fastening points of the paper sheet was 50 mm and the rate of elongation was 12 mm/min.

Table 4. Specifications describing the mechanical strength of the paper, tensile strength

	Sample	PFI beating (revolutions)	Stretch index (Nm/g)	Stretch at break (%)	Tensile breaking load (J/kg)	Tensile stiffness index (kNm/g)	Elasticity module (GPa)
25	REF	0	31.7	3.56	854	3.53	1.70
		1000	44.2	4.73	1487	3.87	2.15
30		2000	61.0	5.61	2297	4.32	2.63
		4000	73.5	5.97	2933	5.15	3.33
		7000	86.7	5.81	3282	5.89	4.06
35	CMC	0	38.4	4.54	1261	3.52	1.88
		1000	72.7	6.19	2832	4.44	2.71
40		2000	89.1	6.03	3382	5.50	3.53
		4000	94.2	6.12	3597	5.72	3.74
		7000	105.1	6.02	3900	6.20	4.31
45	Raisamyl	0	36.9	4.45	1175	3.18	1.56
		4000	83.5	5.98	3271	4.75	3.28

As the table illustrates, the tensile strengths of the laboratory sheets produced from CMC treated pulps were clearly higher than those of corresponding reference tensile strengths. Further, the RBA parameter (relation of bonding fiber area) was higher in the CMC treated pulps than in the reference pulps. Thus, sorption of CMC into the fibers had increased the amount of fiber bonds on a certain pulp beating level.

The tensile strengths of the sheets produced from CMC treated pulp were also considerably higher on a given bonding level than the tensile strengths of reference sheets, i.e. sorption of CMC into the fiber obviously also increased the bonding strength. Further, the stretch at break and tensile breaking load of sheets produced from CMC treated pulps were higher than those of the sheets produced from reference pulps.

4. Internal bond strength

The measurements of the internal bond strength were performed using an Internal Bond Tester meter. The pressure of the tape was 50 lbs/sq.in for unbeaten samples and the samples beaten for 1000 revolutions, 100 lbs/sq.in for samples beaten for 2000 revolutions, 150 lbs/sq.in for samples beaten for 4000 revolutions and 200 lbs/sq.in for samples beaten for 7000 revolutions. The results are presented in figure 7.

The internal bond strengths of sheets produced from CMC treated pulps were considerably higher than the internal bond strengths of sheets produced from corresponding reference pulps, which is most probably due to the increase in characteristic bond strength caused by the sorption of CMC.

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Variable	Mean	SD	Min	Max	Skewness	Kurtosis	Normality
Age	35.2	12.5	18	65	0.15	3.2	0.98
Gender	1.2	0.4	1	2	0.05	3.0	0.99
Marital Status	1.8	0.4	1	3	0.10	3.1	0.98
Education	12.5	2.1	9	16	0.20	3.3	0.97
Income	15000	8000	5000	30000	0.30	3.5	0.96
Occupation	2.5	0.8	1	4	0.15	3.2	0.98
Health Status	1.5	0.5	1	3	0.10	3.1	0.98
Stress Level	3.0	1.0	1	5	0.20	3.3	0.97
Life Satisfaction	4.0	1.2	1	7	0.15	3.2	0.98
Resilience	5.0	1.5	1	7	0.20	3.3	0.97
Optimism	6.0	1.8	1	9	0.15	3.2	0.98
Emotional Stability	7.0	2.0	1	10	0.20	3.3	0.97
Self-Esteem	8.0	2.2	1	10	0.15	3.2	0.98
Life Purpose	9.0	2.5	1	10	0.20	3.3	0.97
Meaning in Life	10.0	2.8	1	10	0.15	3.2	0.98
Existential Well-being	11.0	3.0	1	10	0.20	3.3	0.97
Overall Well-being	12.0	3.2	1	10	0.15	3.2	0.98

1. A method of producing a modified fiber product, according to which method
- cellulosic raw material is formed into a fiber suspension,
 - components modifying the properties of fibers are added to the fiber suspension and
 - the fiber material is dried,
- characterized** in that
- an alkyl derivative of cellulose, which is water-soluble in mainly alkaline conditions, is mixed into the fiber suspension in alkaline conditions, the derivative being at least partly dissolved in water, and
 - the derivative is allowed to be bonded to the fibrous raw material prior to drying the fibrous material so that the bonded cellulose derivative can not be washed off with water.
2. A method according to claim 1, **characterized** in that a paper or paperboard web having good strength properties or good water retention is produced.
3. A method according to claim 1, **characterized** in that a cellulose product having good water retention is produced for use in hygiene products.
4. A method according to any of claims 1 - 3, **characterized** in that the used alkyl derivative of cellulose is carboxymethyl cellulose, carboxyethyl cellulose, methyl cellulose, ethyl cellulose or ether derivatives of any of these.
5. A method according to any of the previous claims, **characterized** in that the alkyl derivative of cellulose is allowed to be sorbed to the cellulose from the water phase so that at least 10 %, preferably 20 %, and especially preferably at least 30 % of the derivative contained by the water phase is allowed to be sorbed to the cellulose.
6. A method according to any of the previous claims, **characterized** in that the pH value of the pulp is more than 8, preferably more than 10.

7. A method according to any of the previous claims, **characterized** in that the pulp is mixed with the cellulose derivative for at least 5 minutes, preferably at least 10 minutes and especially preferably for at least 20 minutes before drying.
- 5 8. A method according to any of claims 1 - 7, **characterized** in that the cellulose derivative to be sorbed is alkali soluble carboxymethyl cellulose (CMC), the DS of which being less than 0.5.
9. A method according to claim 8, **characterized** in that the polymerization degree of the
- 10 CMC is about 600 - 5000.
10. A method according to claim 8 or 9, **characterized** in that the DS of the CMC is 0.2 - 0.4.
- 15 11. A method according to any of claims 1 - 7, **characterized** in that the cellulose derivative to be sorbed is hydroxy-propyl-methyl cellulose (HPMC), hydroxy-ethyl-methyl cellulose (HEMC) and hydroxy-buthyl-methyl cellulose (HBMC).
12. A method according to any of the previous claims, **characterized** in that about 10 %, at
- 20 the most, of the cellulose derivative can be washed off the treated fibrous raw material at a temperature of 25 °C and a neutral pH value.
13. A method according to any of the previous claims, **characterized** in that in comparison with untreated paper, the same internal bond strength is achieved while using at least 10 %
- 25 less pulp.
14. A method according to any of the previous claims, **characterized** in that the cellulose derivative is contacted with the cellulose fibers in an alkaline flow of a pulp or paper mill.
- 30 15. A method according to claim 14, **characterized** in that the cellulose derivative is contacted with the cellulose fibers in an alkaline bleaching stage, such as an oxygen (O) or peroxide (P) stage.

17. A method according to claim 16, **characterized** in that the cellulose derivative is first
5 contacted with chemical pulp, subsequent to which the pulp is drained and the filtrate is
introduced to the peroxide bleaching of mechanical pulp.

10

15 20. A method according to any of the previous claims, **characterized** in that the amount of cellulose derivative is 0.1 to 5 % by weight of the cellulose fibers.

20 and the DS about 0.1 - 0.4.

(57) Abstract:

The present invention relates to a modified fiber product and a method of producing same. According to the method,
5 the cellulosic raw material is formed into a fiber suspension, into which components modifying the properties of the fibers are added, subsequent to which the fibrous material is dried in connection with, for example, web forming. According to the invention, alkyl derivative
10 of cellulose is mixed into the fiber suspension in alkaline conditions, the derivative being at least partly dissolved in water, and the derivative is allowed to be sorbed into the fibrous material prior to drying such that the sorbed cellulose derivative can not be washed off with water. The
15 strength properties or the water retention of paper and paperboard products can be improved by using the invention.

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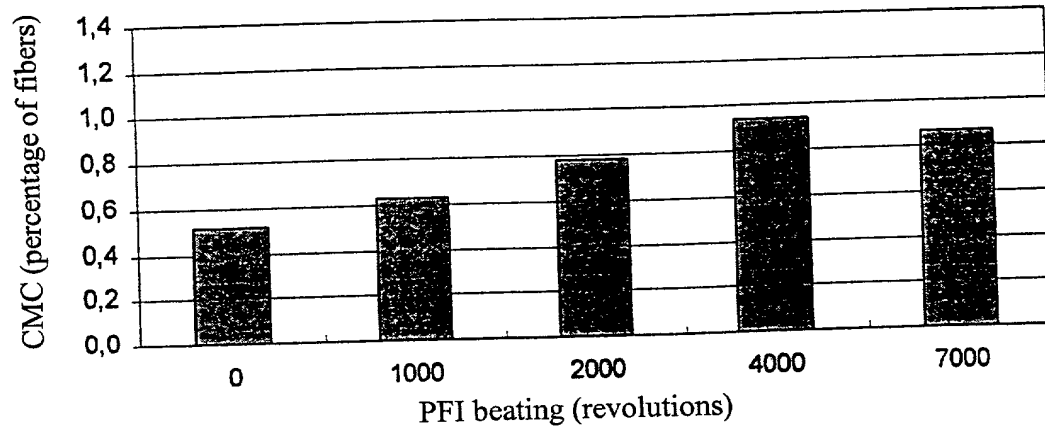


FIG. 1

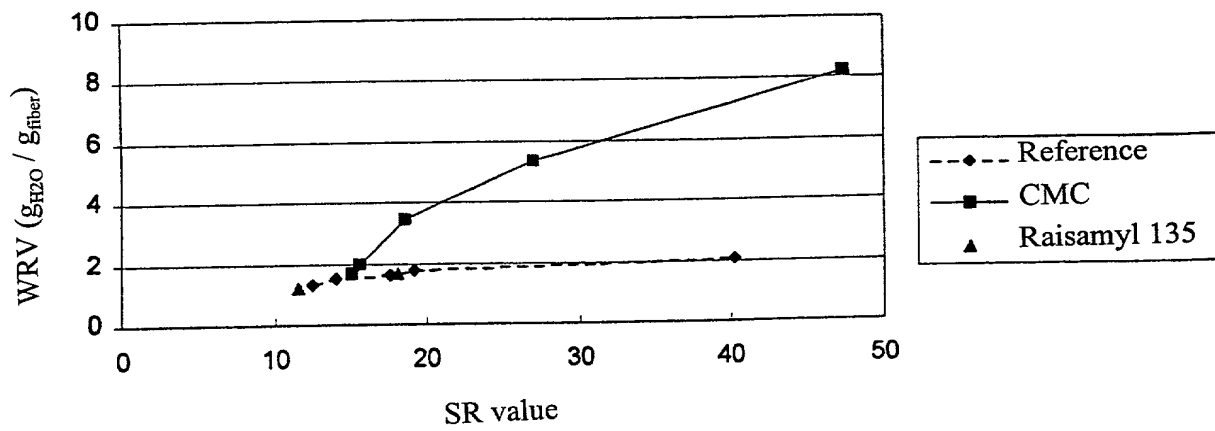


FIG. 2

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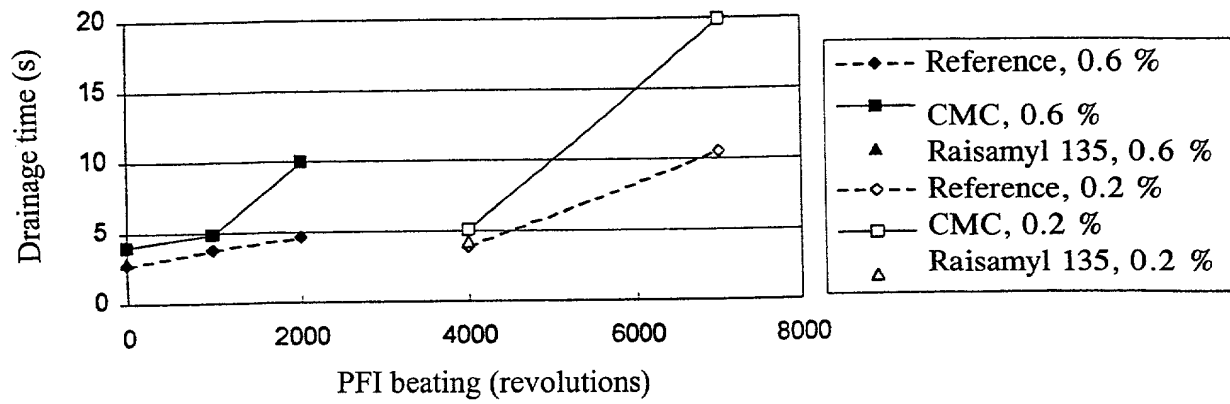


FIG. 3

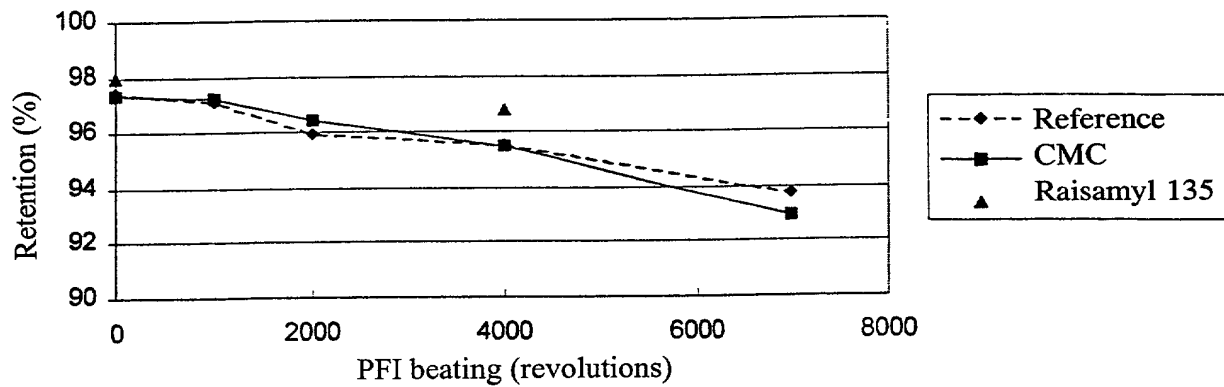


FIG. 4

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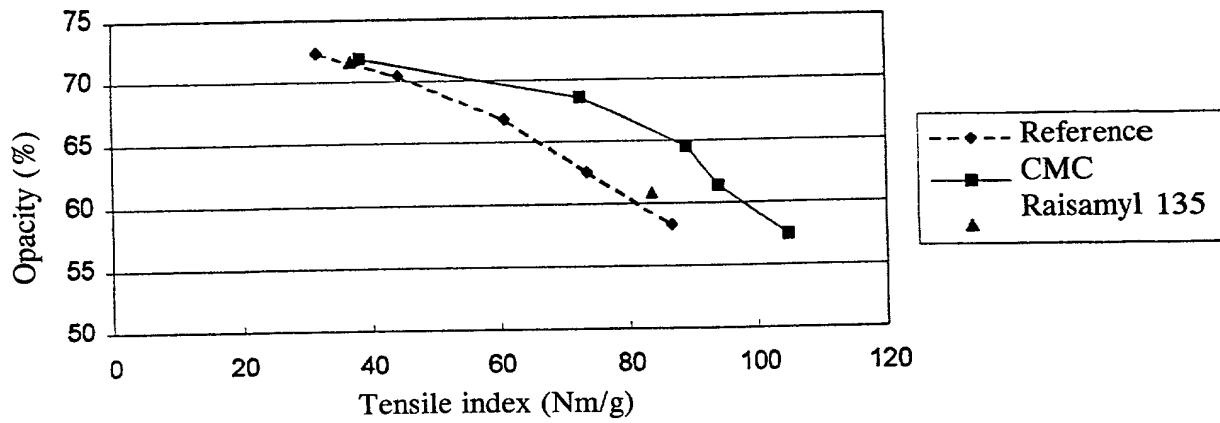


FIG. 5

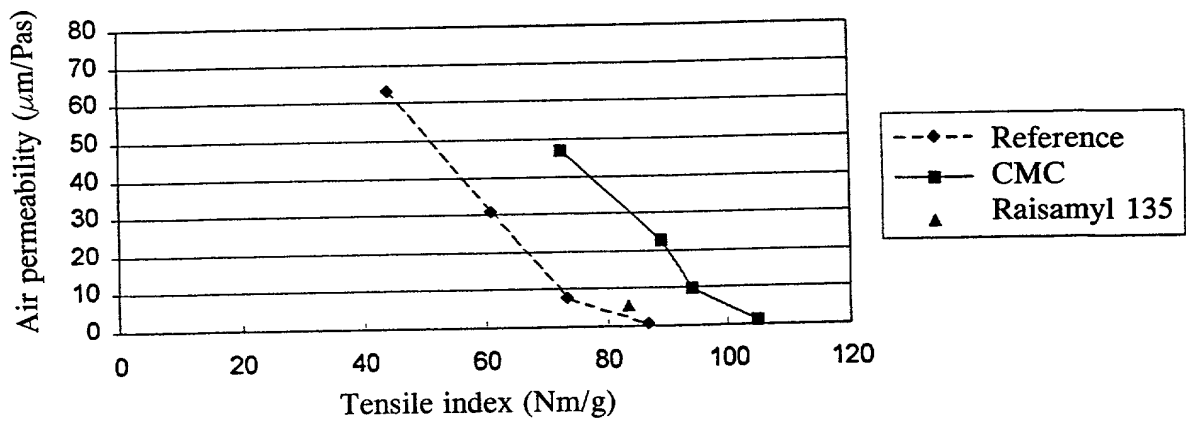


FIG. 6

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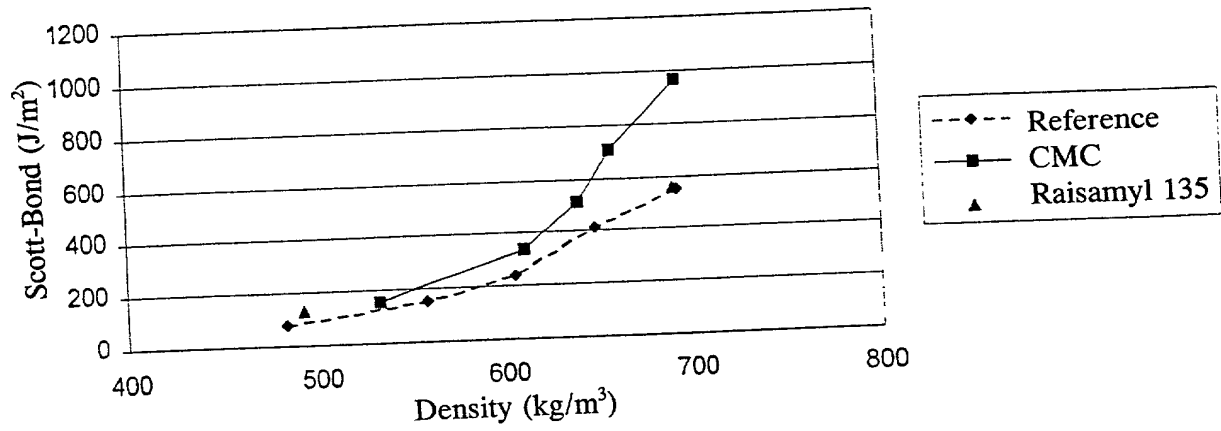


FIG. 7

Declaration For U.S. Patent Application



020374

PATENT TRADEMARK OFFICE

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled (INSERT TITLE) _____

A METHOD OF PRODUCING A FIBER PRODUCT

the specification of which

(Check one
of 1, 2, or
3.)

1. ☐ is attached hereto.
2. ☒ was filed on April 30, 1999 as
International PCT Application No. PCT/FI99/00359
and was amended on _____
(if applicable)
3. ☐ was filed on _____ as
U.S. Application Serial No. _____
and was amended on _____
(if applicable)

I hereby state that I have reviewed and understand the content of the above-identified specification, including the claim(s), as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to the patentability of this application as defined in Title 37, Code of Federal Regulations, §1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, §119 of any foreign application for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application for which priority is claimed:

(List prior
foreign
applications.)

980968
(Number)

Finland
(Country)

30 April 1998
(Day/Month/Year Filed)

Priority Claimed
☒ Yes ☐ No

(Number)

(Country)

(Day/Month/Year Filed)

____ Yes ☐ No

(Number)

(Country)

(Day/Month/Year Filed)

____ Yes ☐ No

☐ See attached list for additional prior foreign applications

I hereby claim the benefit under Title 35, United States Code, §120, of any United States patent application listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulations, §1.56, which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

(Application Serial No.)

(Filing Date)

(Status)

And I hereby appoint as principal attorney and agent Ronald J. Kubovcik, Reg. No. 25,401; and Keiko T. Kubovcik, Reg. No. 40,428.

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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Inventor's Signature: _____ Date: _____

Residence: _____

Citizenship: _____

Post Office Address: _____

Full name of third inventor: _____

Inventor's Signature: _____ Date: _____

Residence: _____

Citizenship: _____

Post Office Address: _____